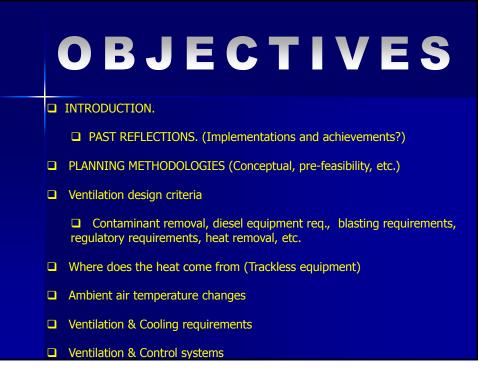
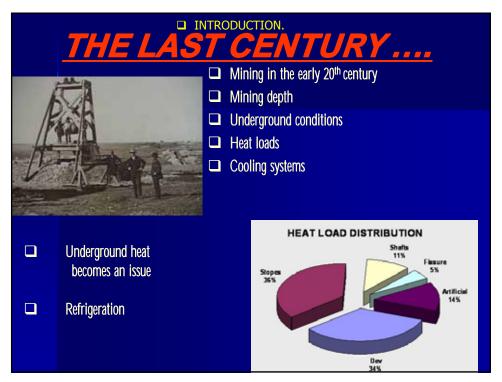
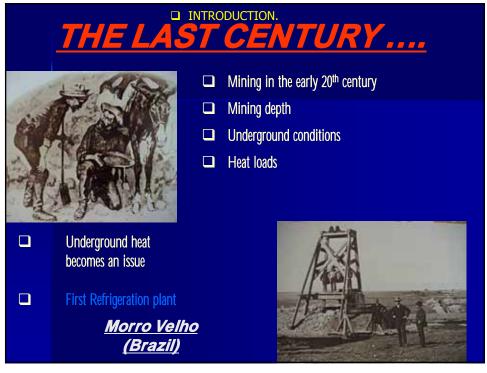
Ventilation Strategies and the use of Trackless equipment MDEC 2004

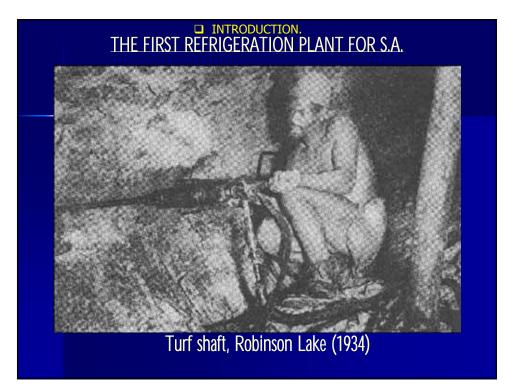
C. Alex Rawlins Ventilation & Refrigeration School of Mining Engineering University of the Witwatersrand

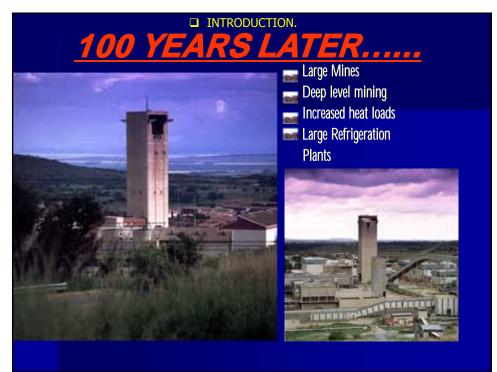




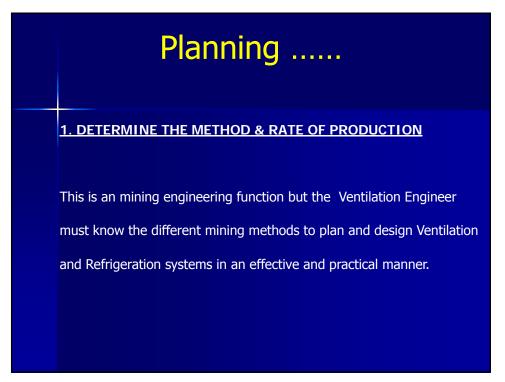


<u>De</u> j	■ INTRODUCTION. Depths reached in Witwatersrand at the end <u>of 1944</u>				
		METRES BELOW SHAFT COLLAR			
	City Deep, 4C Incline	2730			
	Crown Mines, R2 Incline	2647			
	Robinson Deep, 47 – 3 Winze (Turf section)	2630			
	East Rand Proprietary Mine, Angelo Tertiary Incline	2494			
	Durban Roodepoort Deep, 5A Shaft	2395			
	Consolidated Main Reef, 3C Incline	2306			
	Simmer & Jack, East Tertiary	2262			



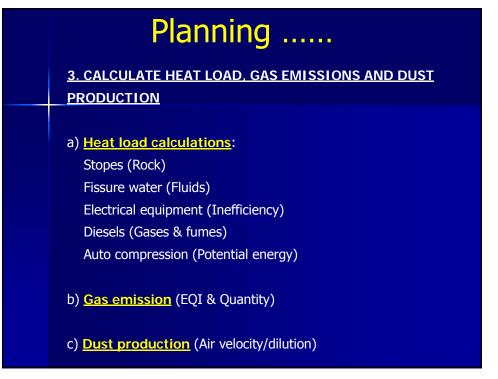








OTHER PARAMETERS Planning 1)Rock thermal conductivity (K – W/mK)) 2)VRT (°C) 3)Rock density $(p - kq/m^3)$ 4)Rock thermal capacity $(C - kJ/kg \circ C)$ 5)Airway length (m) 6)Air quantity (m^3/s) 7) Airway size (m) 8)Pressure (kPa) 9)Years age airway 10)Airway friction factor 11)Insulation thickness (mm) 12)K-Insulation (W/mK) 13)Refrigeration Capital cost (i.e. \$ 1,415/kW) installed 14)Electrical Power Cost (i.e. \$ 170 TO \$ 264/kW) (30% of heat refrigerated) 15)Owning cost time period (i.e. 20 years). 16)Percentage interest used (i.e. 10%) 17)Haualge insulation cost per m³ 18)Psychometric properties (air WB and DB; Barometric pressure, etc.)



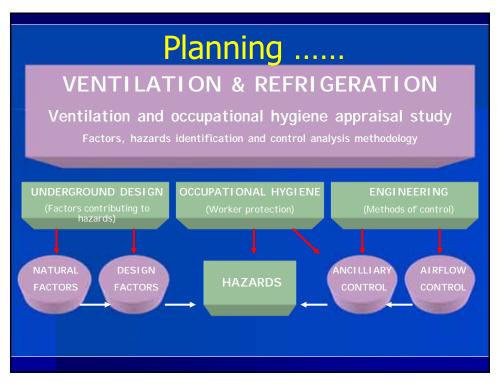


Planning 5. OPTIMISE ALTERNATIVES 6. SELECT SYSTEM

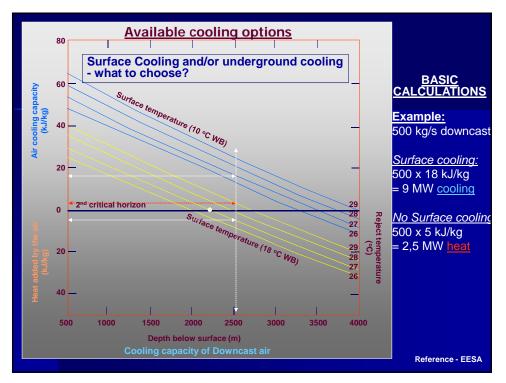
Refrigeration plants can be situated both on surface and underground. What is the fundamental issue when planning a deep underground mine in relation to the location of the plant/s that are needed ?

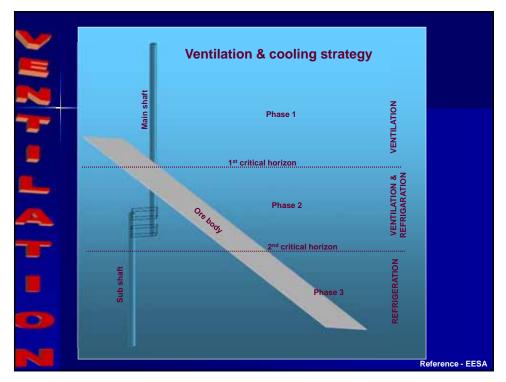
Mining depth
Lateral mining distance from the shaft
Mining area (VRT related)
UG plant has low COP
Use BAC on surface for DC air cooling

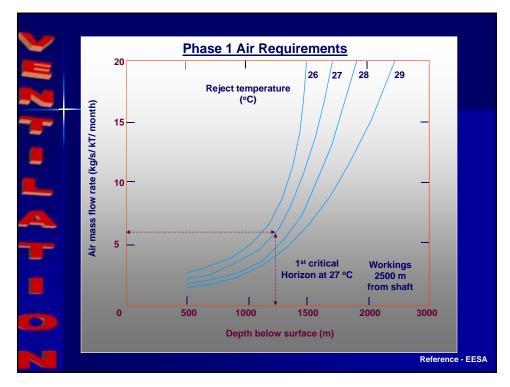
•Use UG plant for deep UG cooling distribution

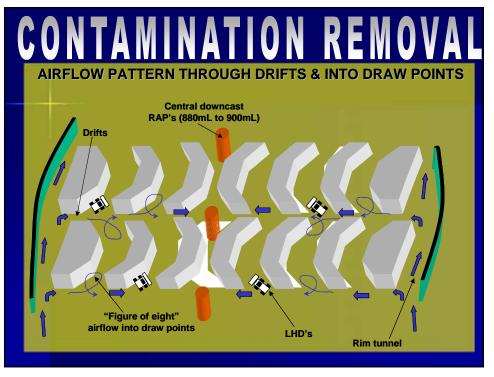


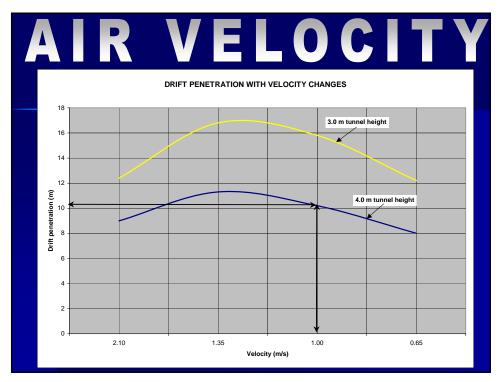


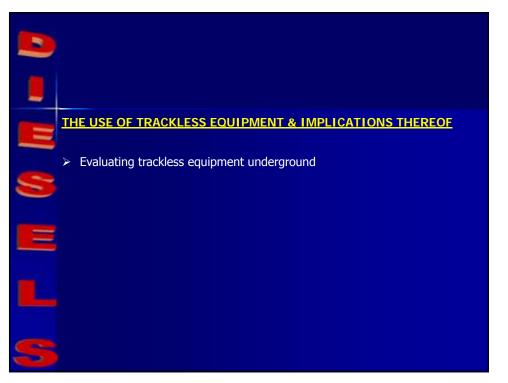














<u>Control:</u> to direct an activity.

<i>Control</i> is considered to be <u>any</u> process whereby the hazard is managed to reduce and maintain the risks at acceptable levels. Here, once again, guidance <u>as to the process should be taken from the MH&SA</u> , Section 11 where the
employer is instructed to assess and respond to risk. In so responding he must, as per Section 11(2):
"determine all measures, including changing the organisation of work and the design of safe systems of work, necessary to eliminate any recorded risk;
control the risk at source; minimise the risk; and in so far as the risk remains – provide for personal protective equipment; and institute a programme to monitor the risk to which employees may be exposed."
The role and <u>duty</u> of the occupational hygienist (Section 12) is therefore to devise appropriate measurement systems which will provide the manager with information which can be used to determine measures or systems which are applied to eliminate , control and minimise health risks and hazards [see sub-section 2(a) and (b)].



Why Ventilation and refrigeration planning?

Overview

□ VENTILATION

Mine ventilation is the continuous supply of <u>adequate</u> and <u>qualitative</u> air to all parts of a mine underground, where people are required to travel or work. This continuous supply of air is required to:

- Supply oxygen for breathing purposes and must be above 19% by volume.
- Remove heat and *provide comfortable working* conditions and hence improve production.
- To dilute and remove noxious and flammable gases that may be encountered during mining operations.
- To dilute and remove hazardous airborne pollutants created by various mining operations underground. (e.g. dust, fumes, aerosols, vapours etc.)
- All these reasons above are to create and maintain an underground working

environment that is conducive to the productivity, health, and safety of people.

2. Overview of current ventilation and refrigeration planning strategies.

Overview

REFRIGERATION

Refrigeration is a process of cooling, whereby heat is removed from a substance (air), where it is not wanted (working places), and put back where it does not affect workers (return airways). It is important to remember that heat is a form of energy and cannot be destroyed, but however can be transferred from one form into another.

In South Africa, refrigeration was introduced for the first time into the gold mines in the 1930's (Turfontein) and the first real increase in capacity occurred during the early 1960's. A dramatic increase in capacity occurred during the mid 1970 - 80's, when refrigeration started to become an integral part of South African modern and ultra deep mining. For example a mine in Free State utilises \pm 105 Mega-watt (105 000 kW) of refrigeration in order to provide comfortable, safe and healthy conditions

underground.

Overview continue....

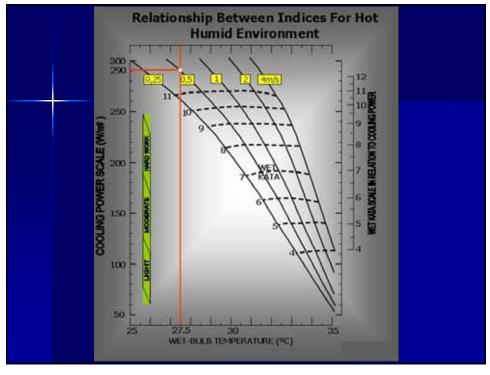
REFRIGERATION

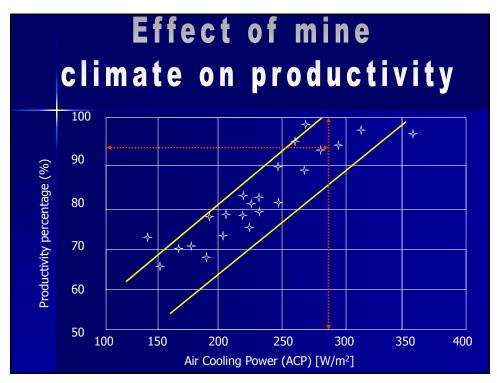
As a general guide in South African gold mines, it is possible to mine down to a VRT of approximately 40°C VRT (\pm 1250m) in most mines, without refrigeration. From 1250 m to \pm 2000 m (40°C+ VRT) the ventilation air is supplemented by refrigeration and beyond 2000 m the air has no residual cooling effect and all the heat produced, must be removed by refrigeration.

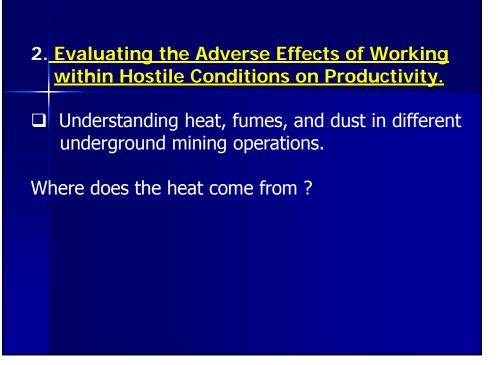
Another guide, which is purely arbitrary and is not based on any fundamental theory of heat exchange, is that 1 kW of refrigeration has the same effect as supplying an extra 0,03 m³/s of air. However, this relationship between air volume flow (m³/s) and unit of refrigeration (kW) is a variable one, and is dependent upon the heat absorption capacity of the prevailing ventilation air. The deeper the higher the station temperature becomes, and under such conditions, refrigeration becomes an essential feature due to

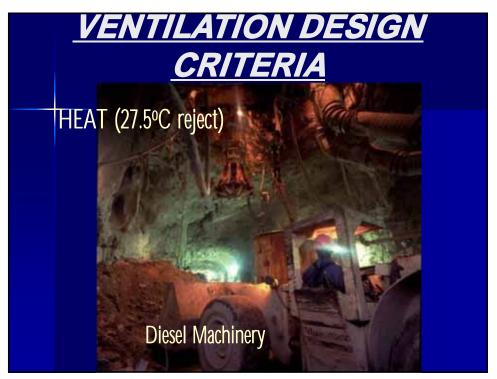
a decrease in the heat absorption capacity of the air.











CANMET for diesel e	A method for calculating the quantity required for a diesel vehicle is the method used by CANMET for diesel engine certification. This method determines an Exhaust Quality Index (EQI). The calculations method is:			
$EQI = \frac{CQ}{50}$	$EQI = \frac{CO}{50} + \frac{NO}{25} + 3.7 \left[\frac{DPM}{2}\right] + 1.5 \left[\frac{SO_2}{3}\right] + 1.2 \left[\frac{NO_2}{3}\right]$			
8	Pollutants and related TLV's from diesel exhaust.			
	Description	Threshold limit value (TLV)		
	Carbon Monoxide (CO)	50 ppm (parts per million)		
	Nitric oxide (NO)	25 ppm		
	Sulphur dioxide (SO ₂)	3 ppm		
	Nitrogen dioxide (NO ₂) 3 ppm			
	Diesel particulate matter (DPM)			

Engines			
 `Nameplating' prevalent in developed world Consider engine choice 			
Sulphur Level (ppm)	Minimum Air Rating (m³/s per kW) "Clean Engine"	Maximum Air Rating (m³/s per kW) "Dirty Engine"	
Low Sulphur 500 ppm	0.0327	0.0668	
High Sulphur 5000 ppm	0.0654	0.1078	
Figures from CANMET nameplate approvals – 150-250 kW range			

Engine type: Detroit Diesel; DDEC 6043-GK32, 5.5I Series 50 ED air requirement: 0.0447 m³/s/kW Fresh Air Quantity (Q) = 187 kW x = 11.22 m³/			
Engine Rating and Maximum Fuel Rate at Sea Level	Sulphur in Fuel - %wt.		
		CFM	m³/s
(205 kW) 275 HP @ 2100 RPM 97.9 lb/hr	0.05 0.10 0.20 0.25 0.50	18 400 20 100 23 300 25 000 33 100	8.7 9.5 11.0 11.8 15.6
(187 kW) 250 HP @ 2100 RPM 91.0 Ib/hr	0.05 0.10 0.20 0.25 0.30 0.50	17 600 19 100 22 100 23 600 27 897 31 200	8.3 9.0 10.4 11.1 13.2 14.7

Diesel consumption for this type of LHD is given as 0.178 L per hour per rated power (kW). Table 3.1.1.2 shows the parameters used in the example.			
Diesel usage (L/hour) Calorific value (kJ/L)			
33.3 35000			
The calculation procedure is: Heat produced = Diesel usage x Calorific value of the diesel / 3600 seconds per hour = 33.3 x 35000/3600 = 323.75 kW This is the total heat produced from the diesel machine and it was imposed that the combustion efficiency is 100%. The heat produced from diesel machinery comprises of both sensible and latent heat. The latent heat component could be calculated from the water produced after combustion at a mean of 1 litre per litre of fuel consumed . Given that the latent heat of evaporation of water is 2450 kJ/kg then the latent heat produced would be 22.7 kW. The sensible component in this example is therefore (323.75 – 22.7) 301 kW. The trackless equipment rated output power would be 187.1 kW. The heat load factor imposed onto the surroundings would be 1.73.			
Depending on the variable parameters used such as the diesel consumption for this specific LHD type, so will the heat load accordingly change. Electrical machinery has the advantage above that of diesel equipment that no latent heat is produced and therefore a reduced heat load component although versatility becomes a problem.			

<u>HEAT</u>				
Diesel fuel usage and parameters				
Diesel usage (L/hour)	Calorific value (kJ/L)			
33.3	35000			
Heat produced = 3 The latent heat = The sensible heat The LHD rated ou The heat load fact	22.7 kW. = 301 kW. tput power = 1	,		

The heat load calculated does not infer that all that heat is available as a source to the ambient surroundings. All would be available if the engine is operating at full capacity all the time, i.e. 100% power utilised constantly. This is generally not the case, and the operating time at full capacity should be monitored and the heat load contribution adjusted to the mean heat load value determined.

For this LHD it is important to determine what the intake WBT just before the LHD should be therefore not to allow the temperature to exceed the design reject temperature of 27.5°C. A simplistic psychrometric calculation is required:

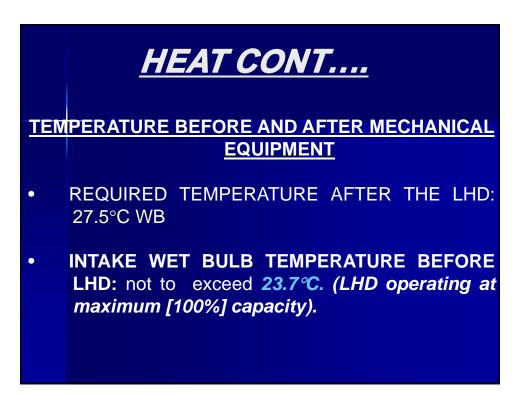
The following parameters are required:

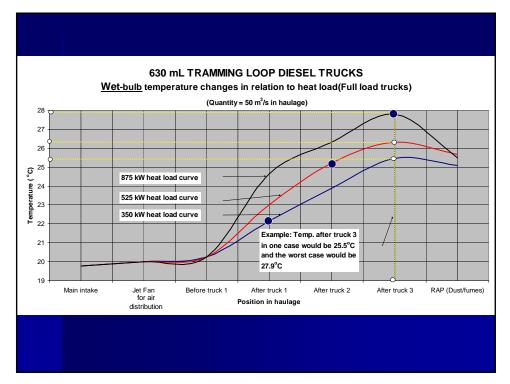
Barometric pressure (P) = 96 kPa Exit temperature after the LHD: 27.5°C WB and say 33°C DB Air mass flow (M_2) = 20 kg/s

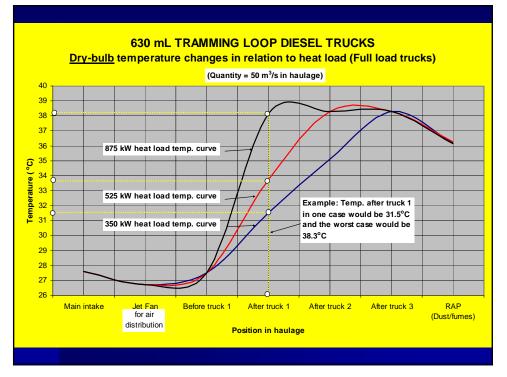
Calculation results are:

The sigma heat value is $(S_2) = 88.15 \text{ kJ/kg}$ The energy content is $(Q_2) = 1763 \text{ kJ/s}$

Therefore, the energy content on the LHD intake side should not exceed (1763 - 323) 1440 kJ/s. This intake energy content corresponds to a sigma (S_2) heat value of 72 kJ/kg. The WBT on the intake side of the LHD should therefore not exceed *23.7°C*. A WBT above **23.7°C before** the LHD (LHD operating at maximum [100%] capacity) would increase the temperature above the design temperature of **27.5°C**.





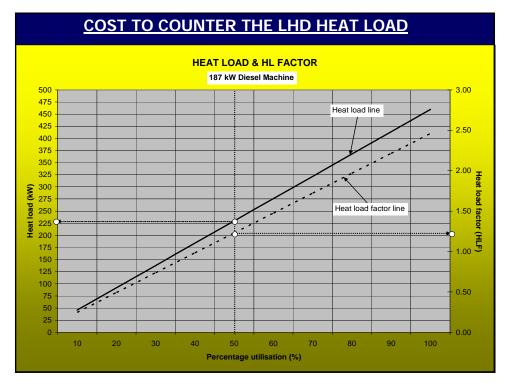


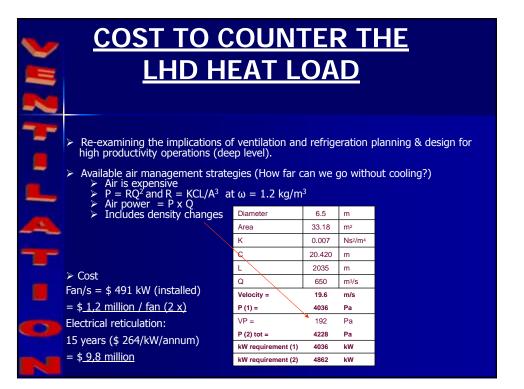
ICE CALCULATION

An example is given to illustrate the unique application of Ice I as used in our mines. The use of ice involves three distinct phases namely (1) from ice at say -3°C to ice at 0°C, (2) when the ice melts at 0°C to form water and (3) the water phase (0°C to say 20°C). Using the specific heat of ice (C) as 2030 J/kg°C the energy transfer calculation is given as follows: Ice mass $(M_i) = 1 \text{ kg}$ Latent heat of melting $(L_i) = 333500 \text{ J/kg}$ Specific heat of water $(C_w) = 4187 \text{ J/kg}^{\circ}\text{C}$ $Q_{ice} = M_i C_i \Delta T$ $Q_{I} = L_{i}M_{I}$ $Q_w = M_w C_w \Delta T$ = 333 500 x 1 = 1 x 2030 x 3 = 1 x 4187 x 20 = 6090 W = 333 500 W = 83 740 W $Q_{tot} = 6090 + 333\ 500 + 83\ 740$ = 423.33 kW per kg of ice The minimum amount of energy available from one kilogram of pure ice would be the

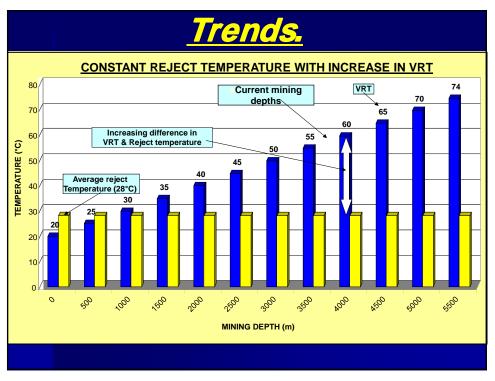
The minimum amount of energy available from one kilogram of pure ice would be the latent energy component namely 333.5 kW. The mass of water required at a supply temperature of say 4°C and return water temperature of 20°C for the same energy transfer would be $\begin{pmatrix} 42330\\ 4187 \times 16 \end{pmatrix}$ 6.3 kg. A ratio of between 1:5 to 1:6 would be general for ice to water mass flow comparisons.

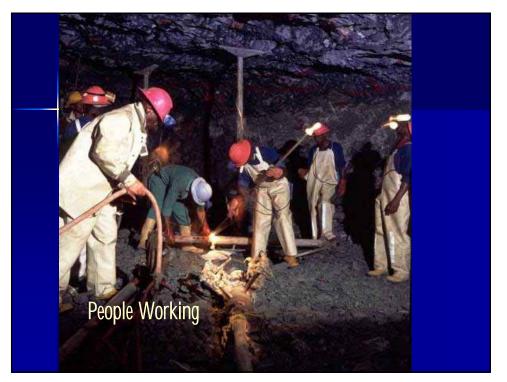
COST TO COUNTER AN LHD'S HEAT LOAD The capital cost of a total refrigeration system is estimated at \$ 1,415/kW(R) and thus, constitutes a one-off payment of \$ 1,840/kW (1,415 x 1.3 = 1,840). (30% losses included) The electrical input power to generate 1.3 kW(R) = 0,39 kW(E) (±30% of kW(R)). The present value (PV) of this power cost over 20 years at 10% = 8.5 Thus: the PV of running costs = (0,39 x 8.5 x \$ 264) = \$ 875/kW (present day electrical power costs are \$ 264/kW/annum including the mean maximum demand). The total owning cost of one kW cooling required is thus, \$ 2.715/kW (\$ 1,840 + \$ 875). For 323.75 kW cooling to be supplied to counter LHD heat the cost would be \$ 879,000 (323.75 x 2,715). Thus approximately 4,8L/s chilled water or 0.76kg ICE



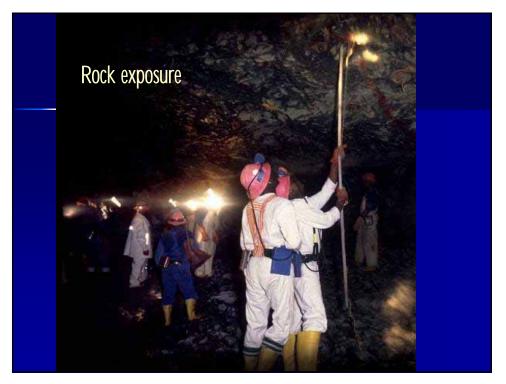


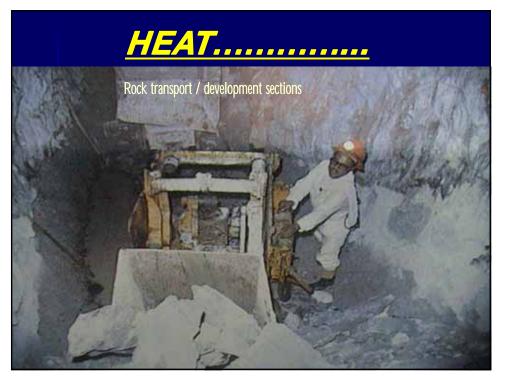






Metabolic rat	Metabolic rates for various activities			
Activity_	Metabolic heat production			
	(W)	M(W/m²)		
Sleeping	73	40		
Seated	107	58.5		
Standing but relaxed	128	70		
Walking on the level at:				
1 m/s	238	130		
1.4 m/s	320	175		
1.8 m/s	403	220		
Manual work				
Very light	174	95		
Light	265	145		
Moderate	448	245		
Heavy	622	340		
		Reference – McPherson (1992)		

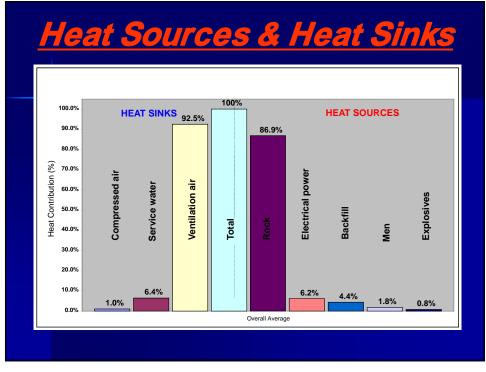


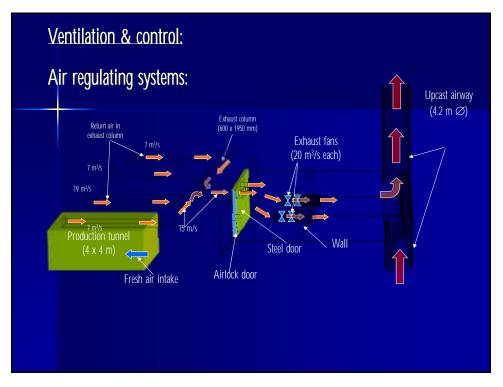


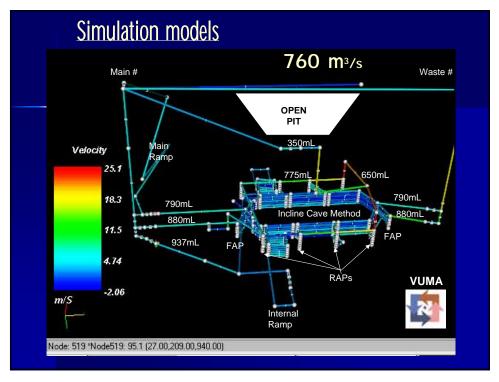
Fissure water is encountered generally in all mining operations, i.e. during shaft sinking, lateral development, etc. The temperature difference between the emitting fissure water and that of the ambient surroundings causes an additional heat load. It therefore makes economical sense and good practice to pipe all return water, i.e. fissure and service water, back to settling dams ready for pumping. An example would be where the difference in the discharge fissure water temperature and the arriving dam water temperature is $(40 - 29) 11^{\circ}$ C. The quantity of fissure water (M_w) is say 20 l/s. The heat ingress into the surroundings would be:



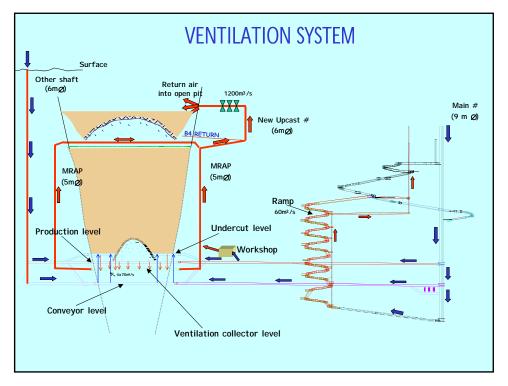
Water has a thermal capacity (C_p) of about 4.187 kJ/kg°C at a temperature of about 15°C.

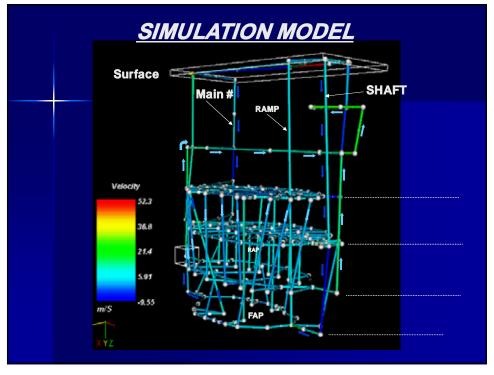






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